

Parameter Estimation of Complicated Thermodynamic Models for Accurate Brine Separation

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 Operations Research
 Laboratory

Motivation



Brine separation is of critical importance to many industries with **brine effluent streams** and/or **brine concentration needs** (e.g., agriculture, power production, mining)

- Reduce costs
- Improve system robustness
- Increase sustainability

Molinari, Raffaele., et al. "Can brine from seawater desalination plants Be a source of critical metals?." CHEMVIEWS (2022).
 Stuber, Matthew D., et al. "Pilot demonstration of concentrated solar-powered desalination of subsurface agricultural drainage water and other brackish groundwater sources." Desalination 355 (2015): 186-196.



Motivation



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[3] Song, Yuhua, et al. "Symmetric electrolyte nonrandom two-liquid activity coefficient model." Industrial & Engineering Chemistry Research 48, no. 16 (2009): 7788-7797.



Refined eNRTL



- Increase accuracy of thermodynamic properties calculation
- Improve accuracy of simulation results





Motivation



Modeling accuracy in high concentration regime

• Refined e-NRTL³

[4] Bollas, G.M., et al. Refined electrolyte-NRTL model: Activity coefficient expressions for application to multi-electrolyte systems. AlChE Journal 54(6): 1608-1624 (2008).



Complexity of Refined eNRTL





[5] Gottlieb, Robert X., et al. "Automatic Source Code Generation of Complicated Models For Deterministic Global Optimization With Parallel Architectures."



Complexity of Refined eNRTL





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Automatic Differentiation Workflow



Number of species in aqueous phase.

Short range excess Gibbs free energy.

Long range excess Helmholtz free energy.

 n_c, n_a, n_m :

 $\mathbf{G}^{\mathbf{SR}}$:

 A^{LR} :



Species with type t, $t \in \{a, c, m\}$ and index j.



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t_i:

R-eNRTL Parameter Estimation



$$egin{aligned} \mathbf{p}^* \in rg\min_{\mathbf{p}\in P\subset \mathbb{R}^{n_p}}\sum_{i=1}^{n_d}(y_i(\mathbf{p})-y_i^{ ext{data}})^2\ ext{s.t.} \quad \mathbf{h}(\mathbf{p}) = \mathbf{0}\ \mathbf{g}(\mathbf{p}) \leq \mathbf{0} \end{aligned}$$

$\mathbf{n}_{c},\mathbf{n}_{a},\mathbf{n}_{m}$:	Number of species in aqueous phase.
G ^{SR} :	Short range excess Gibbs free energy.
A^{LR} :	Long range excess Helmholtz free energy.
$\gamma_{t_j}^{SR}$:	Short Range activity coefficient of species t _j .
$\gamma_{t_j}^{LR}$:	Long Range activity coefficient of species t _j .
t _j :	Species with type t, t $\in \{a, c, m\}$ and index j.
$N_{t_j}^{Data}$:	Experimental data of concentrations of each species.
γ_{\pm}^{Data} :	Experimental data of mean molal activity coefficient
h:	Hydration number of each species, design variables for parameter estimation
τ:	Interaction parameters, design variables for parameter estimation
N_{t_j} :	The concentration of each species in object system

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R-eNRTL Parameter Estimation

EAGO.jl

Deterministic global optimizer

- High performance
- Open-source and free for noncommercial use
- Extensible
- Interval Arithmetic & McCormick based relaxation library

https://www.github.com/PSORLab/EAGO.jl

[7] Wilhelm, Matthew E., and Matthew D. Stuber. "EAGO. jl: easy advanced global optimization in Julia." Optimization Methods and Software 37, no. 2 (2022): 425-450.

$$f(x) = \frac{\exp(x)}{\exp(x)} = 1$$

$$F(X) = \frac{\exp(X)}{\exp(X)} = \left[\frac{\exp(x^{L})}{\exp(x^{U})}, \frac{\exp(x^{U})}{\exp(x^{L})}\right]$$

$$X = [-5, 5] \qquad \Longrightarrow \qquad \left[\frac{\exp(-5)}{\exp(5)}, \frac{\exp(5)}{\exp(-5)}\right]$$

Function Profile (*n*=3)

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Function Profile Animation

 $x_3 = -5 \Rightarrow x_3 = 5$ $x_3 = -5.0$

Interval Extension (n=3)

$$f(\mathbf{x}) = \frac{\mathbf{x}^{\mathrm{T}} \exp(\mathbf{x})}{\mathbf{1}^{\mathrm{T}} \exp(\mathbf{x})} = \frac{x_{1} \exp(x_{1}) + x_{2} \exp(x_{2}) + \dots + x_{n} \exp(x_{n})}{\exp(x_{1}) + \exp(x_{2}) + \dots + \exp(x_{n})} = \sum_{i=1}^{n} \frac{x_{i} \exp(x_{i})}{\sum_{j=1}^{n} \exp(x_{j})}$$

$$f(\mathbf{x}) = \frac{\mathbf{x}^{\mathrm{T}} \exp(\mathbf{x})}{\mathbf{1}^{\mathrm{T}} \exp(\mathbf{x})} = \frac{x_{1} \exp(x_{1}) + x_{2} \exp(x_{2}) + \dots + x_{n} \exp(x_{n})}{\exp(x_{1}) + \exp(x_{2}) + \dots + \exp(x_{n})} = \sum_{i=1}^{n} \frac{x_{i} \exp(x_{i})}{\sum_{j=1}^{n} \exp(x_{j})}$$

$$\sum_{i=1}^{n} \frac{x_{i} \exp(x_{i})}{\exp(x_{1}) + \exp(x_{2}) + \dots + \exp(x_{n})} \cdot \frac{\exp(-x_{i})}{\exp(-x_{i})} = \sum_{i=1}^{n} \frac{x_{i}}{\exp(x_{1} - x_{i}) + \exp(x_{2} - x_{i}) + \dots + \exp(x_{n} - x_{i})}$$

$$\begin{aligned} \mathbf{x}_{i} &= \frac{\mathbf{x}_{i}^{\mathrm{T}} \exp(\mathbf{x})}{\mathbf{1}^{\mathrm{T}} \exp(\mathbf{x})} = \frac{x_{1} \exp(x_{1}) + x_{2} \exp(x_{2}) + \dots + x_{n} \exp(x_{n})}{\exp(x_{1}) + \exp(x_{2}) + \dots + \exp(x_{n})} = \sum_{i=1}^{n} \frac{x_{i} \exp(x_{i})}{\sum_{j=1}^{n} \exp(x_{j})} \\ & \downarrow \\ \sum_{i=1}^{n} \frac{x_{i} \exp(x_{i})}{\exp(x_{1}) + \exp(x_{2}) + \dots + \exp(x_{n})} \cdot \frac{\exp(-x_{i})}{\exp(-x_{i})} = \sum_{i=1}^{n} \frac{x_{i}}{\exp(x_{1} - x_{i}) + \exp(x_{2} - x_{i}) + \dots + \exp(x_{n} - x_{i})} \\ & \sum_{i=1}^{n} \frac{x_{i}}{\exp(x_{1} - x_{i}) + \exp(x_{2} - x_{i}) + \dots + \exp(x_{n} - x_{i})} \\ & \Rightarrow f(\mathbf{x}) = \sum_{i=1}^{n} \frac{x_{i}}{1 + \sum_{\substack{j=1\\j \neq i}}^{n} \exp(x_{j} - x_{i})} \end{aligned}$$

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$$f(\mathbf{x}) = \frac{\mathbf{x}^{\mathrm{T}} \exp(\mathbf{x})}{\mathbf{1}^{\mathrm{T}} \exp(\mathbf{x})} = \frac{x_{1} \exp(x_{1}) + x_{2} \exp(x_{2}) + \dots + x_{n} \exp(x_{n})}{\exp(x_{1}) + \exp(x_{2}) + \dots + \exp(x_{n})} = \sum_{i=1}^{n} \frac{x_{i} \exp(x_{i})}{\sum_{j=1}^{n} \exp(x_{j})}$$

$$\sum_{i=1}^{n} \frac{x_{i} \exp(x_{i})}{\exp(x_{1}) + \exp(x_{2}) + \dots + \exp(x_{n})} \cdot \frac{\exp(-x_{i})}{\exp(-x_{i})} = \sum_{i=1}^{n} \frac{x_{i}}{\exp(x_{1} - x_{i}) + \exp(x_{2} - x_{i}) + \dots + \exp(x_{n} - x_{i})}$$

$$\sum_{i=1}^{n} \frac{x_{i}}{\exp(x_{1} - x_{i}) + \exp(x_{2} - x_{i}) + \dots + \exp(x_{n} - x_{i})}$$

$$\Rightarrow f(\mathbf{x}) = \sum_{i=1}^{n} \frac{x_{i}}{1 + \sum_{\substack{j=1\\ j \neq i}}^{n} \exp(x_{j} - x_{i})}$$

$$\Rightarrow Alche 2023$$

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$$X_1, X_2, X_3 = \begin{bmatrix} -5, 5 \end{bmatrix}$$

$$f(\mathbf{x}) = \frac{\mathbf{x}^{\mathrm{T}} \exp(\mathbf{x})}{\mathbf{1}^{\mathrm{T}} \exp(\mathbf{x})}$$

$$F X = \left[3 \frac{-5 \exp(5)}{\exp(-5)}, 3 \frac{5 \exp(5)}{\exp(-5)} \right]$$
$$\approx \left[-3 \times 10^5, 3 \times 10^5 \right]$$

$$f(\mathbf{x}) = \sum_{i=1}^{3} \frac{x_i}{1 + \sum_{j=1, j \neq i}^{n} \exp(x_j - x_i)} \implies F X = \begin{bmatrix} 3 \frac{-5}{1 + 2\exp(-5 - 5)}, 3 \frac{5}{1 + 2\exp(-5 - 5)} \\ \approx \begin{bmatrix} -15, 15 \end{bmatrix} \end{bmatrix}$$

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$$X_{1}, X_{2}, X_{3} = \begin{bmatrix} -5, 5 \end{bmatrix}$$

$$f(\mathbf{x}) = \frac{\mathbf{x}^{\mathrm{T}} \exp(\mathbf{x})}{\mathbf{1}^{\mathrm{T}} \exp(\mathbf{x})} \implies F X = \begin{bmatrix} 3 - 5 \exp(5), 3 5 \exp(5) \\ 7 \times 5 \end{bmatrix}$$

$$f(\mathbf{x}) = \sum_{i=1}^{3} \frac{x_{i}}{1 + \sum_{j=1, j \neq i}^{n} \exp(x_{j} - x_{i})} \implies F X = \begin{bmatrix} 1 + 5 \exp(5), 3 5 \exp(5) \\ 7 \times 5 \exp(5) \end{bmatrix}$$
Interval shrunk by **4**
orders of magnitude
$$F X = \begin{bmatrix} 1 + 5 \exp(5), 3 5 \exp(5) \\ 7 \times 5 \exp(5) \end{bmatrix}$$

McCormick Relaxations

Parameter Estimation Result

using JuMP, EAGO, ForwardDiff import JuMP.@variable as @variable new_fun = functionalize_obj_NaCl_fast(expr) objfun(t1,t2,hc11,ha11) = objfun_eval_single_y^{s R}_NaCl_fast(new_fun,t1,t2,hc11,ha11) factory = () -> EAGO.Optimizer(SubSolvers()) model = Model(optimizer_with_attributes(factory, "absolute_tolerance" => 1e-4,"time_ register(model,:objfun,4,objfun,autodiff=true) lb =[0. -10. 0. 0.] ub = [10. 0. 2. 2.] @variable(model, lb[i]<= x[i=1:4] <= ub[i]) @NLobjective(model, Min, objfun(x[1], x[2], x[3], x[4])) @NLconstraint(model, y1, x[3]-x[4]>=0) optimize!(model)

✓ 9m 45.1s

Parameter Estimation Result

Absolute Tolerance Achieved First Solution Found at Node 1029 LBD = 0.0 UBD = 5.977314675518958e-6 Solution is: X[1] = 7.834167504201094 X[2] = -3.907172657309239 X[3] = 1.5789380575987575 X[4] = 0.723255866122256

Scalability

Interaction Parameter

Conclusions

- Implemented refined eNRTL model for single electrolyte case and generated activity coefficients as symbolic expressions using AD.
- Reformulated problematic multivariate quotient term to significantly reduce overestimation of dependency problems.
- Demonstrated the new rule by solving the parameter estimation problem for aqueous NaCl using EAGO.
- Currently implementing the multi-electrolyte form and expanding the AD work for all other thermodynamic properties

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Questions

https://www.psor.uconn.edu

Thermodynamic of Refined eNRTL

A Novel, Tight Interval Extension Rule

$$f(\mathbf{x}) = \frac{\mathbf{x}^{\mathrm{T}} \exp(\mathbf{x})}{\mathbf{1}^{\mathrm{T}} \exp(\mathbf{x})} = \frac{x_1 \exp(x_1) + x_2 \exp(x_2) + \dots + x_n \exp(x_n)}{\exp(x_1) + \exp(x_2) + \dots + \exp(x_n)}$$

$$=\frac{x_1 \exp(x_1)}{\exp(x_1) + \exp(x_2) + \ldots + \exp(x_n)} + \frac{x_2 \exp(x_2)}{\exp(x_1) + \exp(x_2) + \ldots + \exp(x_n)} + \ldots + \frac{x_n \exp(x_n)}{\exp(x_1) + \exp(x_2) + \ldots + \exp(x_n)}$$

$$=\frac{x_1 \exp(x_1) + \exp(x_2) + \ldots + \exp(x_n)}{1 + \exp(x_2 - x_1) + \ldots + \exp(x_n - x_1)} + \frac{x_2}{\exp(x_1 - x_2) + 1 + \ldots + \exp(x_n - x_2)} + \ldots + \frac{x_n}{\exp(x_1 - x_n) + \exp(x_2 - x_n) + \ldots + 1}$$

$$= \sum_{i=1}^n \frac{x_i}{1 + \sum_{j=1, j \neq i}^n \exp(x_j - x_i)}$$

